

# SIZE REDUCTION

# Size Reduction

- **Size reduction** : The process of converting the object from one physical dimension of higher order to another dimension of smaller.
- **Comminution** is another term used for size reduction

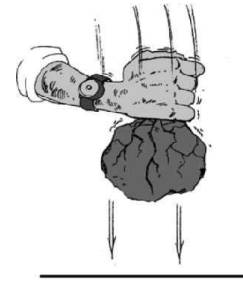
## Objectives of Size Reduction

- To increase the **surface area**
- To get the desired **shape, size or size ranges** and **specific surface** particles
- To separate **unwanted particles** effectively
- To dispose **solid waste** easily
- To **mix** solid particles more **intimately** and
- To improve the **handling (storage and transportation)** characteristics

## Methods

### Impact

- The particle is subjected to a **single violent force**.
- **Instantaneous collision** of one moving object against another
  - Both objects may be moving, Ex: Cricket bat connecting with a fast moving ball
  - One object may be motionless, Ex: Rock being struck by a hammer below



**Impact  
(hammer)**

**Gravity impact:** The free falling material is momentarily stopped by the stationary object

Ex: coal dropped onto a hard steel surface

- Most often used when it is necessary to separate relatively different friable materials

**Friable:** Something that is crumbly is easily broken into lot of little pieces

- The more friable is broken first, while the less friable remains unbroken

**Dynamic impact:** Ex: Materials dropped in front of a moving hammer

- The material is unsupported and the force of impact accelerates movement of the reduced particles towards the breaker plate and/or other hammers.
- Needed for cubical particles, materials are too hard and abrasive and the product must meet intermediate size specifications

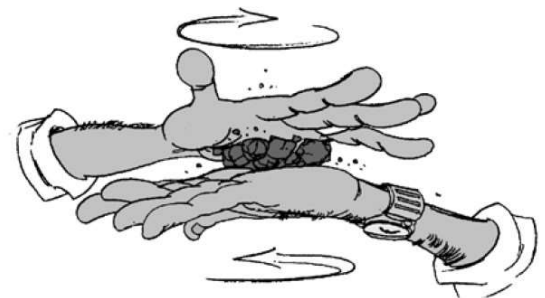
## Compression

- The particle is broken by **two forces** and the size reduction is done between two surfaces with the work being done by one or both the surfaces.
- **Jaw crushers using this method** of size reduction are suitable for reducing extremely hard and abrasive rock.
  - Both objects may be moving, Ex: Cricket bat connecting with a fast moving ball
  - One object may be motionless, Ex: Rock being struck by a hammer below

**Chosen:** The free falling material is momentarily stopped by the stationary object

Ex: coal dropped onto a hard steel surface

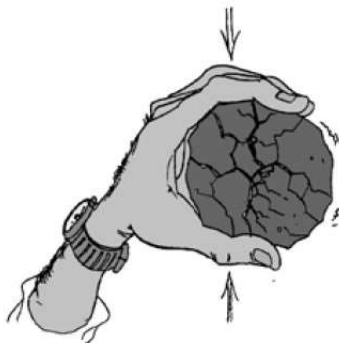
- If the material is **hard** and **tough**
- If the material is **abrasive**
- If the material is **not sticky**
- If the finished product is to be relatively **coarse** in size
- When the material will **break cubically**



**Attrition (file)**

## Attrition

- **Rubbing or scrubbing** the materials between two surfaces.
- Hammer mills operate with the close clearance between the hammers and screen bars, reduce the size of the materials by **attrition combined with shear and impact actions**.
- Though it consumes more power , it is **proffered** for crushing the **less abrasive** materials such as limestone and coal.
- It is most **useful** when the material is **friable** or **not too abrasive** and a closed circuit system is not desirable to control the oversize.

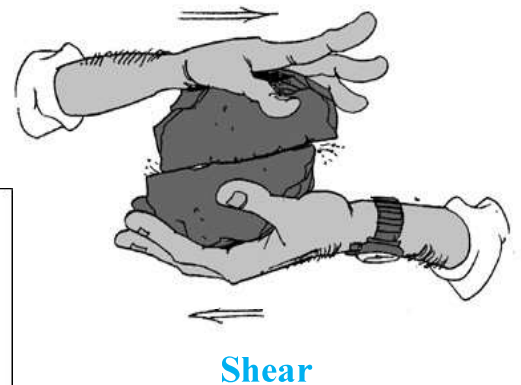
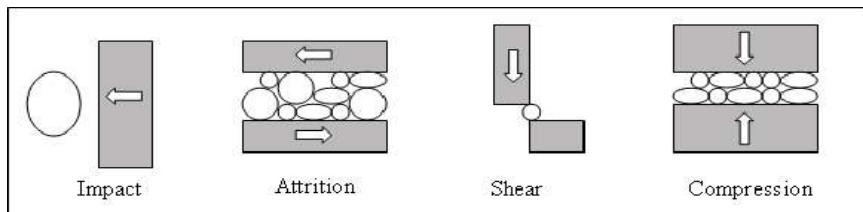


**Compression  
(nutcracker)**

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# Shear

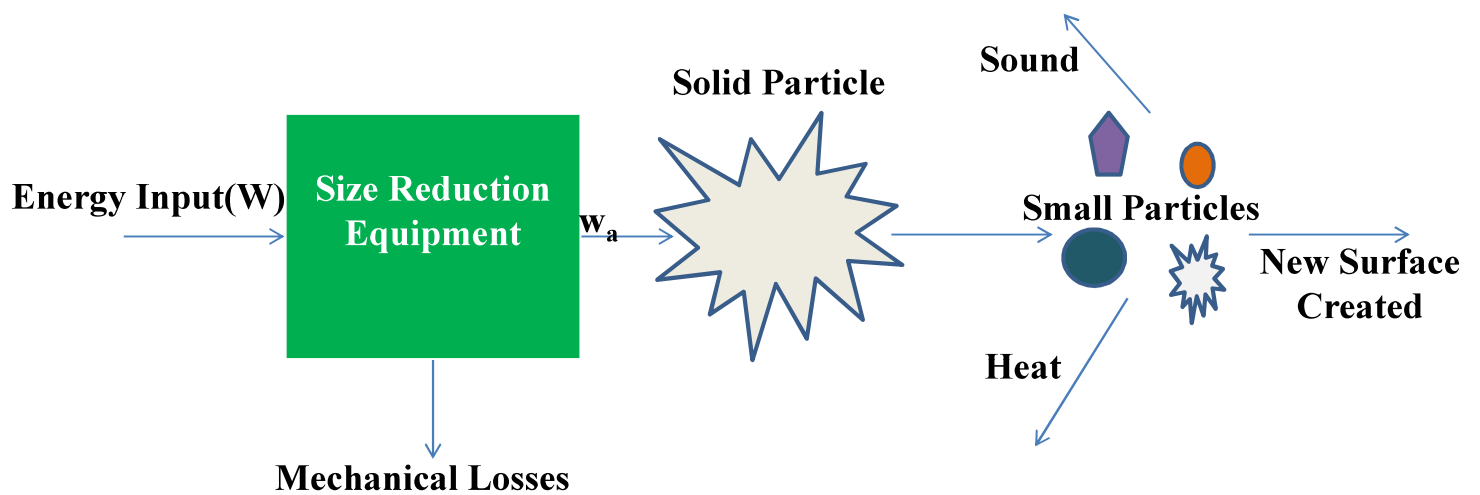
- **Trimming or cleaving** action rather than rubbing action associated with attrition.
- It is usually combined with other size reduction actions.  
Ex: Single roll crushers employ shear together with impact and compression.
- It is needed for friable material , primary crushing with a reduction ratio of 6 to 1 and
- Production of relatively coarse product.



## **Factors affecting the size reduction process**

- a) Presence of moisture and sticky materials in equipment's feed
- b) Presence of fines in the feed
- c) Segregation of feed particles in the crushing chamber
- d) Lack of feed control
- e) Wrong motor size
- f) Insufficient crusher discharge area
- g) Insufficient capacity of the crusher's discharge conveyor
- h) Materials being extremely hard to crush
- i) Surface energy of solids
- j) Power consumption
- k) Selection of an appropriate crushing chamber

# Energy and Power Consumption



# Crushing Efficiency

- The ratio of surface energy created to the energy absorbed by the solid.
- The ratio of energy absorbed by the solid to form heat and energy input to the machine
- Range: 0.001 to 1 %.
- **Quantities needed:**
- **Total energy input** : Measured either by mechanical means or by electrical instruments
- **Energy lost during size reduction** : difficult to measure but may be measured in terms of energy consumption
- **Total new surface created**: determined by size distribution or by flow through a powder bed or by the adsorption of gas molecules on the powder surface , gas diffusion, and heats of adsorption
- **Specific surface energy** : indirect methods based on mathematical utilization of physicochemical quantities

# Determination of Power Consumption

$$\eta_c = \frac{\text{Surface energy created by crushing}}{\text{Total energy absorbed by the solid}}$$

- $W_a$  = Total energy absorbed by a unit mass of solid, J/Kg
- $E_s$  = Surface energy per unit area, J/m<sup>2</sup>
- $A_{ssf}, A_{ssp}$  = Areas per unit mass of feed and product respectively (Specific Surfaces), m<sup>2</sup>/kg
- The surface energy created by crushing will be  $E_s (A_{ssp} - A_{ssf})$

$$\eta_c = \frac{E_s (A_{ssp} - A_{ssf})}{W_a} \rightarrow W_a = \frac{E_s (A_{ssp} - A_{ssf})}{\eta_c}$$

- Mechanical Efficiency :  $\eta_m = \frac{\text{Total energy absorbed by the solid}}{\text{Total energy fed to the machine}} = \frac{W_a}{W} \rightarrow W = \frac{W_a}{\eta_m}$

$$W = \frac{E_s (A_{ssp} - A_{ssf})}{\eta_m \eta_c}$$

$$P = W \cdot m$$

$$P = \frac{E_s (A_{ssp} - A_{ssf}) m}{\eta_m \eta_c}$$

$$P = \frac{6E_s m}{\left[ \frac{1}{\eta_m \eta_c} - \frac{1}{\eta_m \eta_c} \right]}$$

$$A_s = \frac{6}{\Phi \rho_p D_{vs}}$$

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# Laws of Communion

**Rittinger's Law :** The work required for size reduction is proportional to the new surface area created.

$$W_R = \frac{P}{m} = KE_s (A_{ssp} - A_{ssf})$$

$$W_R = \frac{P}{m} = 6 KE_s \left[ \frac{1}{\Phi_p D_{vsp} \rho_{pp}} - \frac{1}{\Phi_f D_{vsf} \rho_{pf}} \right] \quad K = \frac{1}{\eta_c}$$

$$W_R = \frac{6 KE_s}{\Phi_p \rho_p} \left[ \frac{1}{D_{vsp}} - \frac{1}{D_{vsf}} \right] = K_R \left[ \frac{1}{D_{vsp}} - \frac{1}{D_{vsf}} \right]$$

## *Rittinger's Nun*

**Kick's Law :** The work required for crushing a given mass of material is constant for a given reduction ratio irrespective of the initial size.

$$W_K = \frac{P}{m} = K_K \ln \left[ \frac{D_{vsf}}{D_{vsp}} \right]$$

## Laws of Communiton

**Bond's Law :** The work required to form particles of size  $D_{pp}$  from a very large particle size is proportional to the square root of the surface to volume ratio of the product.

$$W_B = \frac{P}{m} = K \left[ \sqrt{\frac{S_P}{V_P}} \right] = K \left[ \sqrt{\frac{6}{\Phi_p D_{pp}}} \right] = K \sqrt{\frac{6}{\Phi}} \left[ \sqrt{\frac{1}{D_{pp}}} \right] = K_B \sqrt{\frac{1}{D_{pp}}}$$

$$W_B = \frac{P}{m} = K_B \left[ \sqrt{\frac{1}{D_{pp}}} - \sqrt{\frac{1}{D_{pf}}} \right]$$

**Work Index:** the gross energy requirement in kilowatt hour per short-ton of feed (kWh/ton of feed) to reduce a very large particle to such a size that 80% of the product will pass through a 100  $\mu\text{m}$  or 0.1 mm screen.

$$W_B = \frac{P}{m} = 0.3162 W_i \left[ \sqrt{\frac{1}{D_{pp}}} - \sqrt{\frac{1}{D_{pf}}} \right]$$

**Generalized Law :**

$$d(W) = d\left(\frac{P}{m}\right) = -K \frac{d(D_{vs})}{D_{vs}^n}$$

(n = 2, 1 and 1.5 for Rittinger's , Kik's and Bond's laws respectively)

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# Size Reduction Equipment

## 1. Mode of operation

- a) Batch operated
- b) Continuous operated

## 2. Method by which a force is applied

### → Impact

- a) Impact at one surface
- b) impact between particles

### → Compression between two solid surfaces

- a) Crushing
- b) Grinding

### → Rubbing the materials between two solid surfaces

## 3. Size of Feed and Product

## 4. Cutting machines - cutting

- a) Knife cutters, dicers, slitters

# Types of size reduction equipment

	Feed	Product
<b>1. Crushers</b>	large pieces into small lumps	
a) Primary crusher	very large lumps, run-of-mine material	150 to 250 mm
b) Secondary crusher	takes product from primary crusher	6 mm
<b>2. Grinders</b>	reduce crushed feed to powder	
a) Intermediate grinders		40 mesh screen
b) Fine grinders		200 mesh screen
<b>3. Ultrafine grinders</b>	Accepts feed < 6 mm	1 to 50 $\mu\text{m}$
<b>4. Cutters</b>		Definite size and shape (2 to 10 mm in length)

# Classification of Size Reduction Equipment

## 1. Crushers (coarse & fine) - compression

- a) Jaw crusher
- b) Gyratory crusher
- c) Crushing rolls

## 2. Grinders (Intermediate & fine) - impact & attrition

- a) Hammer mills and impactors
- b) Rolling-compression mills
  - (i) Bowl mills
  - (ii) Rolling mills
- c) Attrition mills
- d) Revolving/Tumbling mills
  - (i) Rod mills (ii) Ball mills; pebble mills, and (iii) tube mills

## 3. Ultrafine grinders - attrition

- a) Hammer mills with internal classification
- b) Fluid-energy mills
- c) Agitated mills

## 4. Cutting machines - cutting

- a) Knife cutters, dicers, slitters

# Crushers

- Slow speed machines for coarse reduction of large quantities of solids
- They operate by compression
- Can break large lumps of hard materials
- Find application in rockery and mining industries
- Types:
  - a) **Jaw crusher**
  - (i) **Blake jaw crusher**
  - (ii) **Dodge jaw crusher**
  - b) **Gyratory crusher**
  - c) **Smooth-roll crusher**

## Jaw Crushers

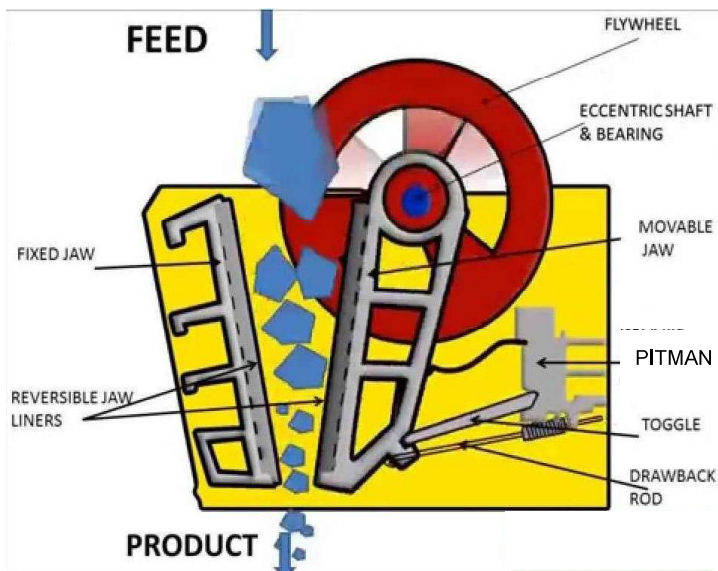
- Compress the feed between a stationary jaw and a movable jaw
- (i) **Blake jaw crusher** : movable jaw is pivoted at the top, maximum movement at the bottom



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# Blake Jaw Crusher - Construction

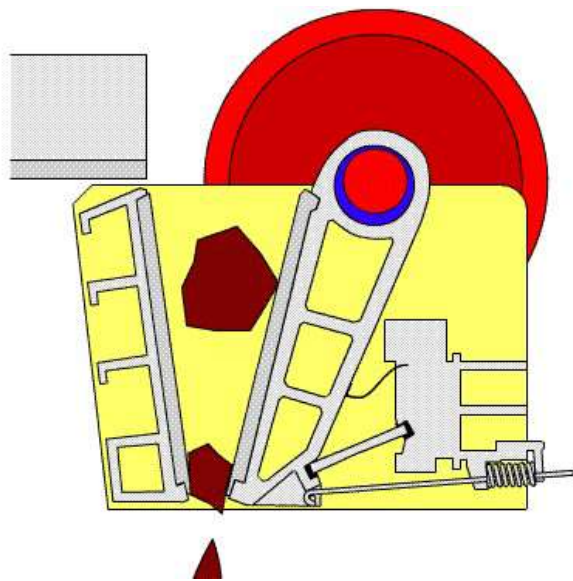
Working principle: **Compression**



- Fixed jaw and movable jaw (pivoted at top) form V-open
- Swinging jaw reciprocates in horizontal plane, makes an angle of 20-30° with the nearly vertical fixed jaw
- Jaws made of manganese steel to withstand abrasion
- Faces usually corrugated
- Eccentric- causes vertical oscillation of pitman, communicated horizontally (reciprocating motion) to the movable jaw by toggles
- Speed of operation - should not be high since fines cannot escape

**Protection:** 2 toggles held by bolts that shear first, failure at easily repairable point

## Blake Jaw Crusher - Working



- Material caught between upper part of jaws is crushed into smaller size during forward motion by compression
- Crushed material falls into narrow space during backward motion and is recrushed
- Crushed material drops out from bottom
- Jaws open and close at 250-400 times/min

- Maximum movement of the jaw at the discharge end, less choking
- Loading is uneven, so heavy flywheel

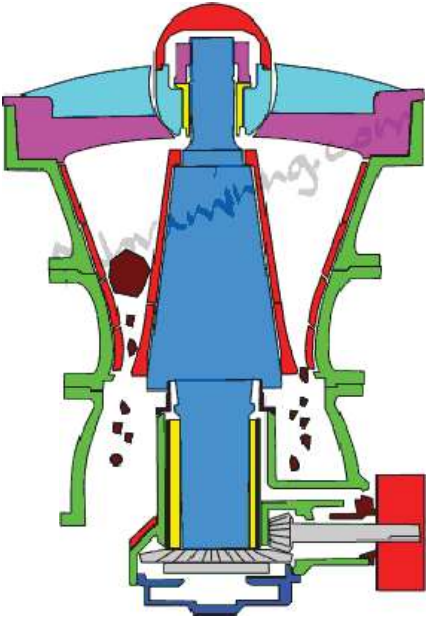
### Eccentric



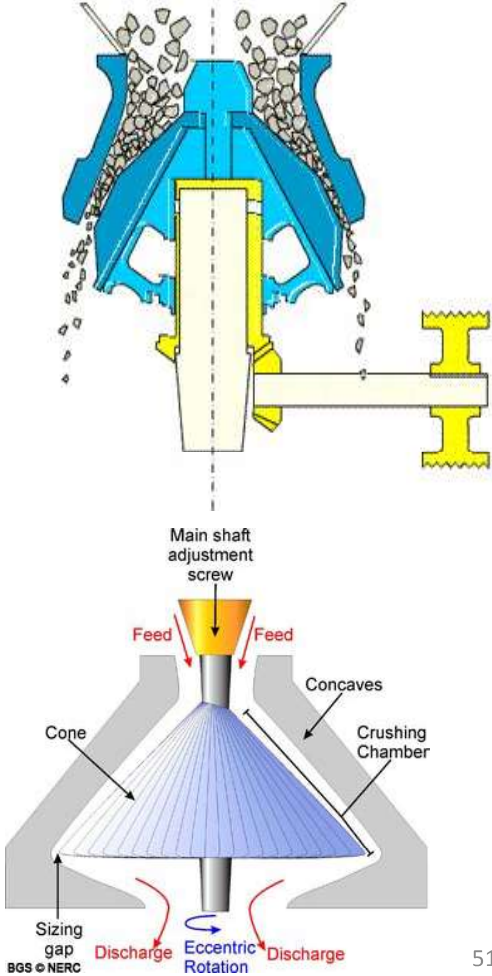
## **Blake Jaw Crusher**

- Movable jaw is pivoted at top
- Maximum movement at bottom
- No tendency to choke/clog
- Suitable for higher production rates
- Large reduction ratio is not possible
- Low maintenance
- Made in larger sizes
- Does not give uniform product
- Widely used

# Gyratory Crusher

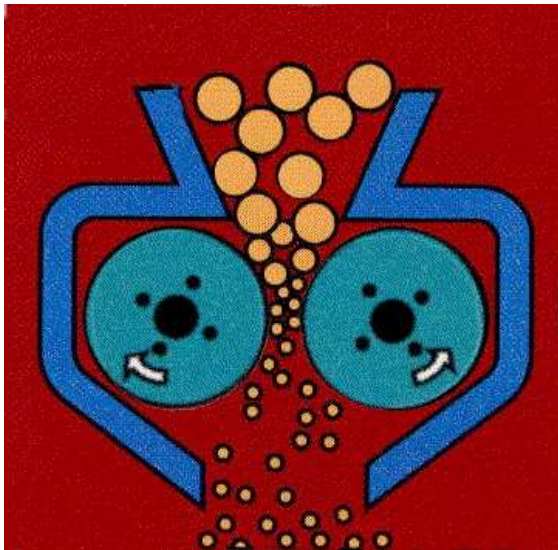


# Cone Crusher

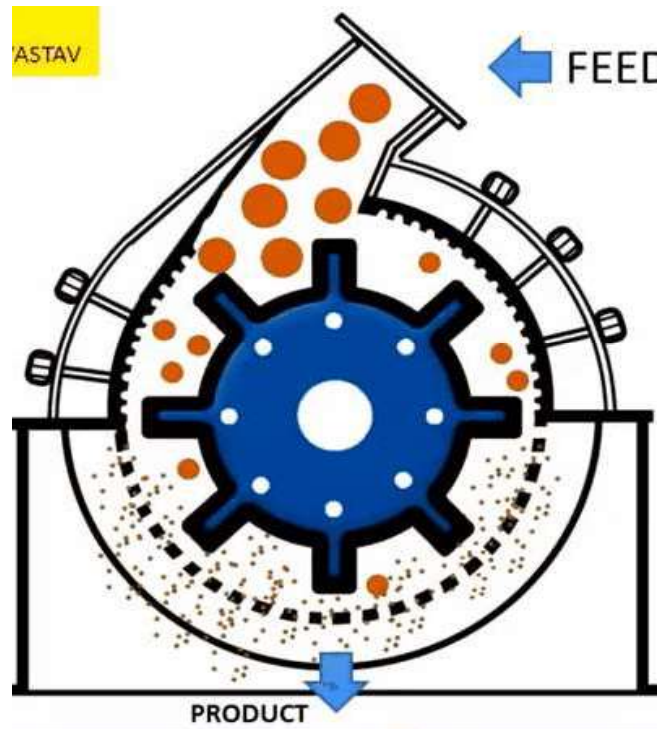


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# Roll Crusher



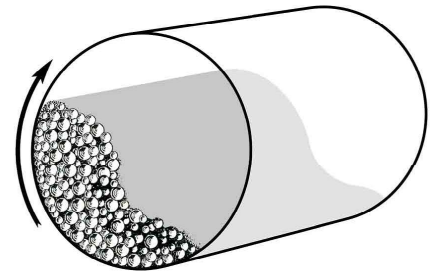
# Grinders - Edge Runner Mill and Hammer Mill



## Revolving / Tumbling Mills

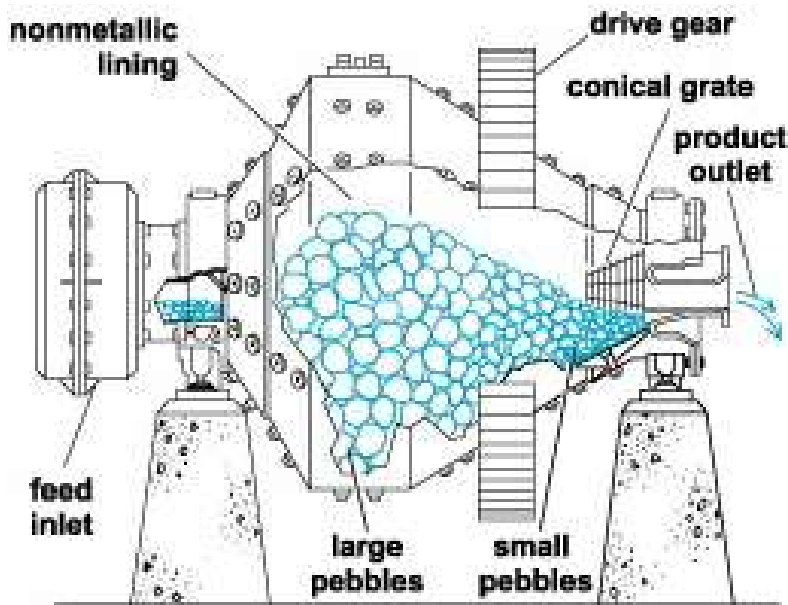
- Cylindrical shell slowly rotating on horizontal axis and charged with grinding medium to about half its volume
- Shell - steel; Lined with abrasion resistant materials (manganese steel, ceramic, or rubber)
- Operation - (a) Batch, (b) Continuous

Type	Reduced by	Grinding Medium
<b>Ball mill</b> ( $L=D$ )	Impact	Steel balls/ rubber/wood
Tube mill ( $L \geq 2D$ )	Impact	Smaller balls (finer product)
Rod mill	Rolling, compression, attrition	Steel rods
Pebble mill	Impact	Flint/ceramic pebbles



# Ball Mill - Construction

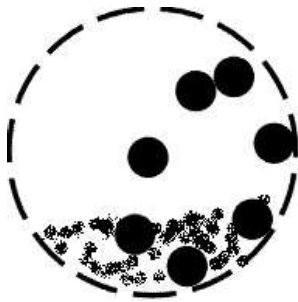
Principle: **Impact**  
(when balls drop from near the top of shell)



- Batch or continuous, wet or dry operation
- Large ball mill (3 m diameter, 4.25 m length)

- Hollow cylindrical shell (horizontal or slightly inclined) rotating about its axis at low speed using a drive gear (60 to 100 rpm)
- Length = diameter of mill
- Inner lining - abrasion resistant manganese steel or rubber
- Partially filled with balls made of steel, stainless steel or rubber
- Coarse screen at outlet - to prevent escape of balls
- **Balls**
  - - occupy 30 to 50 % of mill volume
  - - Diameter 12 to 125 mm
  - - Optimum ball diameter =  $\sqrt{\text{Feed size}}$

## Ball Mill - Working



### Continuous Operation

- Feed - from left through 60° cone; Product discharge - from 30° cone to the right
- Balls rise and then drop on feed; Solids are ground and reduced in size by impact
- When shell rotates, large balls segregate at feed end, small balls near product end
- Initial breaking – by large balls dropping from largest distance
- Small particles – by small balls from short distance
- If rate of feed ↑ coarse product obtained ↑
- If speed of rotation ↑ fineness for given capacity

### Batch Operation

- After feeding, close opening
- Mill is rotated for a fixed time
- Stop mill and discharge product

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# Ball Mill

Applications:

To grind coal, pigments, and feldspar for pottery

**WET GRINDING** - at low speeds

- Low power consumption ( 20 to 30 % less than dry grinding)
- High capacity
- Dust reduction
- Necessary to dry the product
- High wear on grinding medium (20 % higher than dry grinding)

**Factors influencing product size:**

- a) Feed rate
- b) Properties of feed material
- c) Weight of balls
- d) Speed of rotation of mill
- e) Level of material in the mill

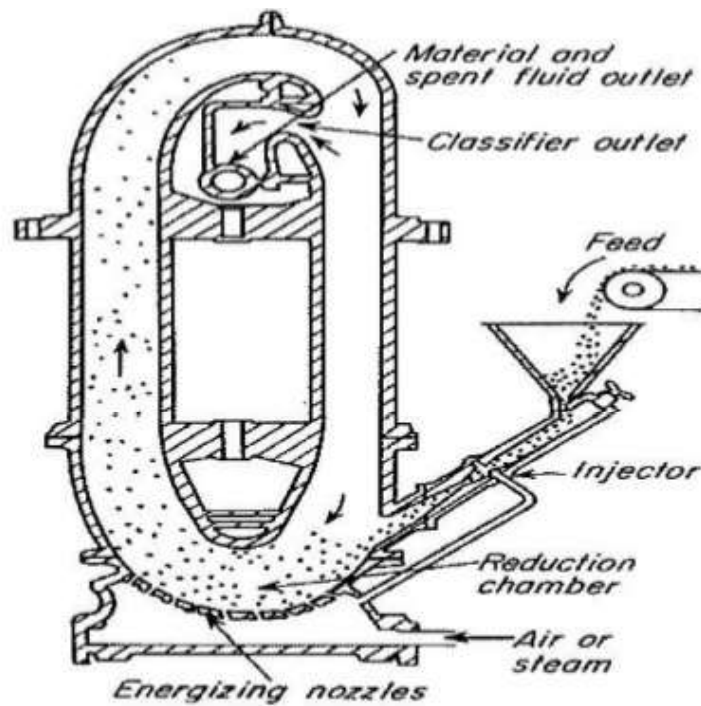
**BALL MILL - ADVANTAGES**

- Low installation cost
- Low power requirement
- Suited for all degrees of hardness
- Batch, continuous mode
- Open, closed circuit grinding
- Explosive materials ground in inert atmosphere
- Grinding medium - cheap

## Action in Tumbling Mills

- During upward movement of balls - balls + wall in contact due to centrifugal force (some grinding due to slipping and rolling)
- Maximum grinding - when free falling ball strikes bottom by impact
- Balls are projected across mill depending on speed of rotation
  - Low speed – balls simply roll over - little crushing
  - High speed- balls carried up in mill & greater power consumption (greater impact, larger capacity)
  - Very high speed – balls carried round in contact with sides & mill is **centrifuging**
  - Minimum speed at which centrifuging occurs - **critical speed of mill** (centrifugal force will be exactly balanced by weight of ball)
  - Little or no grinding when mill is centrifuging
  - Operating speed = 50 to 75 % of critical speed
  - **Critical speed,**  
R- radius of mill  $N_c = \frac{1}{2\pi} \sqrt{\frac{g}{R-r}}$   
r- radius of ball  
g - acceleration due to gravity

## Ultrafine Grinders - Fluid Energy Mills



# Effective Methods for Operating

- **Open Circuit Grinding:** One or more grinding mills arranged in series or parallel without classification equipment. This method discharges a final ground as it comes from a mill and there is no return of coarse discharge back to the mill.
- Conditions that favor open circuit grinding are small reduction ratios, coarse reduction of particles.
- **Closed Circuit Grinding:** Consists of one or more grinding mills with classification equipment. The mills discharge ground product to classifier which returns the coarse product from it to the mill for further grinding.
- Conditions that favor closed circuit grinding are larger reduction ratios and finer reduction of particles.
- **Advantages:** higher capacity, lower power consumption, fine to ultrafine, avoids coarse material in final product, eliminates overgrinding of fines.

## **Size Reduction Equipment in Industry**

- 1) Jaw crusher - cement industry
- 2) Ball mill - paint industry
- 3) Ultrafine grinders - Cosmetic, pharmaceutical
- 4) Cutters - Leather tanning
- 5) Hammer mill - Food industry